

**Executive Order VR-203-D**  
**VST Phase II EVR System**

**Exhibit 2**  
**System Specifications**

This exhibit contains the installation, maintenance and compliance standards and specifications that apply to the VST Phase II EVR System installed at a gasoline dispensing facility (GDF). All components must be installed, maintained, and operated in accordance with the specifications in the **ARB Approved Installation, Operation and Maintenance Manual (IOM)**. Installation, maintenance and repair of system components, including removal and installation of such components in the course of any required tests, shall be performed by technicians certified by the appropriate manufacturer. Additional certifications may be required in accordance with local district requirements. Provided that there are no other local district requirements, a GDF owner/operator can remove and install nozzles, curb hoses, breakaways, and whip hoses without a manufacturer certification.

**Nozzle**

1. A vapor collection sleeve shall be installed on the nozzle at the base of the spout, as shown in **Figure 2B-1**.
2. The VST Model VST–EVR-NB nozzle has an integral vapor valve which prevents the loss of vapor from the underground storage tanks, ensures proper operation of the system and prevents the ingestion of air into the system. The performance of the nozzle vapor valve can be determined by items 2.1 or 2.2.
  - 2.1. The maximum allowable leak rate for the nozzle vapor path, as determined by TP-201.2B, shall not exceed 0.07 cubic feet per hour (CFH) at a pressure of two inches water column (2.00" WC)
  - 2.2. Verification of the integrity of the vapor valve can be performed on installed nozzles using the nozzle bag test procedure in Exhibit 10.
3. The gasoline flow rate of the nozzle shall be between six (6.0) and ten (10.0) gallons per minute as determined by the applicable provisions of section 6 or 7 of Exhibit 5 or by direct observation for 30 seconds minimum at the maximum hand held position.

**Vapor Collection**

1. The system pressure drop from the nozzle to the UST, as determined by TP-201.4 (Methodology 1), shall not exceed the following:

0.35 inches WC at a flow rate of 60 CFH of Nitrogen; and  
0.62 inches WC at a flow rate of 80 CFH of Nitrogen.

### **Coaxial Hoses**

1. The maximum length of the curb hose, breakaway, and whip hose combined shall not exceed fifteen feet as measured from the base of the nozzle to the end of dispenser adapter or dispenser, as appropriate.
2. The liquid removal rate shall not be less than five milliliters per gallon (5 ml/gal) as determined by Exhibit 5 when tested with a gasoline flow rate between six (6.0) and ten (10.0) gallons per minute. Liquid removal requirement is applicable to all grade of gasoline.
3. Any hose configuration is allowed when installed in accordance with IOM section 12.

### **Breakaway Couplings**

1. The VST breakaway couplings are non-reconnecting and shall be replaced following a drive-off. If reusing hanging hardware other than the breakaway following a drive-off, testing is required to ensure proper operation and no observed leaks of the hanging hardware prior to returning the fueling point to operation. The procedure for testing the hanging hardware following a drive-off is referenced in the IOM section titled "Drive-offs and Other Customer Abuse."

### **Flow Limiter**

1. No flow limiter is allowed for this system.

### **VST ECS Membrane Processor**

1. The processor vapor integrity shall demonstrate compliance with the static pressure decay criteria of TP-201.3 and Exhibit 4.
2. Unless there is maintenance or testing being conducted on the processor, the processor shall be on and in the automatic vapor processor mode and the three ball valves shall be locked in the open positions shown in **Figure 2B-2** for normal processor operation. The handles of the ball valves shall not be removed.
3. Piping to and from the processor shall be sloped 1/8" per foot minimum toward the vent line(s).
4. The hydrocarbon concentration of the ECS membrane processor taken from the Hydrocarbon Diagnostic Report shall be between  $\pm$  one percent ( $\pm 1\%$ ), when tested in accordance with Exhibit 6.
5. The Vapor Pressure Sensor shall be between +0.2 and -0.2 inches WC when tested in accordance with section 9 of Exhibit 8.

6. The processor shall activate when the pressure of the underground storage tank is less than or equal to 0.4 inches WC ( $\leq 0.4$  inches WC) as determined by Exhibit 9.
7. The ECS Membrane Processor alarm shall activate when the emission factor is at or greater than 0.64 pounds/1000 gallons dispensed over a 24 hour period. A visual and audible alarm shall activate when this emission factor is exceeded for the first and second 24 hour periods.
8. The pressure reading from the TLS console shall be within  $\pm 0.2$  inches WC of the measured ullage UST pressure as determined by section 8 of Exhibit 8.
9. The ECS Membrane Processor audible alarm shall be installed at a location that is most likely to be occupied by the station attendant during normal station operation (i.e., cash register).
10. The TLS console controlling the membrane shall have an RS232 port which shall be installed in a location that allows the RS232 port to be easily accessible, and if applicable per district requirements, for use at anytime. A vacant RS232 serial port shall always be available to electronically download reports.

#### **Veeder-Root Vapor Polisher**

1. The carbon type shall be BAX G1500 manufactured by MeadWestvaco.
2. Unless there is maintenance or testing being conducted on the processor, the vapor polisher shall be on and in the automatic vapor processor mode and the inlet ball valve shall be locked in the open position shown in **Figure 2B-3** for normal polisher operation. The handle of the ball valve shall not be removed.
3. The pressure reading from the TLS console shall be within  $\pm 0.2$  inches WC of the measured ullage UST pressure as determined by section 8 of Exhibit 8.
4. The Vapor Pressure Sensor shall be between +0.2 and -0.2 inches WC when tested in accordance with section 9 of Exhibit 8.
5. The Vapor Polisher leak rate difference between starting and ending pressures shall be less than 0.5 inches WC loss when tested in accordance with Exhibit 11. The ending pressure must be greater than 7.0 inches WC. Pressure drop across the Vapor Polisher at 18.7 standard cubic feet per hour flow shall be between 1.8 inches WC and 2.4 inches WC when tested in accordance with Exhibit 11. Differences in temperature readings shall not exceed 10 °F when tested in accordance with Exhibit 11. The atmospheric pressure sensor reading shall be within 10% of the atmospheric pressure obtained from a local independent source when tested in accordance with Exhibit 11.
6. The hydrocarbon concentration from the vapor polisher outlet shall not exceed 0.9% by volume iso-butane (9,000 ppmv or 50% of the lower explosive level (LEL)) when tested in accordance with Exhibit 12.

7. The TLS console controlling the vapor polisher shall have an RS232 port which shall be installed in a location that allows the RS232 port to be easily accessible, and if applicable per district requirements, for use at anytime. A vacant RS232 serial port shall always be available to electronically download reports.
8. Security seal tags must be installed on the vapor polisher. If for any reason the seal tags are damaged or missing, the district may require that Exhibit 11 and Exhibit 12 be conducted and pass prior to installing new security seal tags.

#### **Pressure/Vacuum Vent Valves for Storage Tank Vents**

1. Except for the P/V vent valve referenced in item 3 of this section, all P/V vent valves shall be an ARB certified P/V valve for a Phase I system.
2. At least one pressure/vacuum (P/V) vent valve shall be installed on each tank vent. The maximum number of P/V vent valves allowed and P/V vent valve performance specifications are listed in the applicable Phase I EVR Executive Order. Vent lines may be manifold to minimize the number of P/V vent valves and potential leak sources, provided the manifold conforms to all applicable fire regulations. However, the vents connecting the vapor inlet and vapor outlet to the VST ECS Membrane Processor cannot be manifold together.
3. The P/V valve installed on the VST ECS Membrane Processor vent is not part of the Phase I system and no testing is required.

#### **Vapor Recovery Piping Configurations**

**NOTE: Vapor Return Piping shall meet the requirements specified in section 4.11 of CP-201.**

1. Vapor Return and Vent Lines

For facilities installed on or after April 1, 2003, all vapor return and vent lines shall be a minimum nominal internal diameter of 2 inches from the dispensers or the vent stacks to the first manifold. All lines after the first manifold and back to the underground storage tank shall have a minimum nominal internal diameter of 3 inches.

Note: Facilities permitted by a local district prior to April 1, 2003 shall be required to meet the three inch diameter standard only upon facility modification which involves the addition, replacement, or removal of 50 percent or more of the buried vapor piping.

2. All vapor return lines shall have a minimum slope of 1/8 inch per foot from the dispenser riser to the riser of the UST. A slope of 1/4 inch or more per foot is recommended wherever feasible.

3. The dispenser shall be connected to the riser with either flexible or rigid material that is listed for use with gasoline. The dispenser-to-riser connection shall be installed so that any liquid in the lines will drain toward the storage tank. The internal diameter of the connector, including all fittings, shall not be less than one inch (1").

Note: The dispenser-to-riser connection is defined as the piping connection between the dispenser piping and the inlet of the dispenser riser. A vapor shear valve may also be part of the riser connection.

4. There is no length restriction for the vapor return piping of the system as long as the system complies with the maximum pressure drop requirement, item 1 of the Vapor Collection section.
5. No product shall be dispensed from any fueling point at a GDF installed with the VST Phase II EVR System if there is a vapor line that is disconnected and open to the atmosphere.
6. No liquid condensate traps are allowed with this system.

### **Dispensers**

1. For new installations and existing installations replacing dispensers or dispenser vapor piping, the minimum nominal internal diameter of dispenser vapor piping shall be one inch (1" ID). For existing installations, installed dispenser vapor piping may remain in use as long as the system complies with the maximum pressure drop requirement, item 1 of the Vapor Collection section.
2. Dispenser vapor piping shall be installed so that any liquid in the lines will drain toward the dispenser riser.

### **Phase I System**

1. The Phase I system shall be an ARB-certified system that demonstrates compliance with the static pressure decay test criteria contained in TP-201.3 and Exhibit 4.

### **Maintenance Records**

1. Each GDF operator owner shall keep records of alarms and maintenance performed at the facility. Such records shall be maintained on site in accordance with district requirements or policies. The records shall include alarm date and time, nature of the alarm, troubleshooting, maintenance or repair performed to validate and/or correct alarms, component, or system failures, date when maintenance or repair was conducted, name and Certified Technician Identification Number of individual conducting maintenance or test, affiliation, and telephone number. Additional information may be required in accordance with local district requirements. An example of a GDF maintenance and alarm record is shown in Figure 2B-4.
2. Maintenance shall be conducted in accordance with the Scheduled Maintenance section of the ARB approved Installation, Operation, and Maintenance Manual.

### **Vapor Recovery Equipment Defects**

The following is deemed a defect for the affected fueling point(s) or system.

#### Fueling Points

1. The fueling point shall be removed from service when more than 30% of a nozzle face seal is missing (e.g., a triangular or similar shape in which greater than 2.5 inches of the faceplate circumference is missing (accumulated)).
2. The fueling point shall be removed from service when more than 0.375 square inches of a nozzle vapor collection sleeve is missing (e.g., a rectangular shape of greater than nine/sixteenth (9/16) inches or more on each side, a circular shape of eleven/sixteenth (11/16) inches or more in diameter, or a triangular shape of seven/eighth (7/8) inches on the side.
3. The fueling point shall be removed from service when the total slit length in the convolutions exceeds 18 inches as determined by direct measurements.
4. The fueling point shall be removed from service when a hose is found to have greater than 175 ml of gasoline in the vapor side as determined by sections 6.1 to 6.5 of Exhibit 5. Note: Prior to draining gasoline from the vapor side of the VST hose, use VST tool P/N VST-STP-100 and plug the fuel spout. **Do not activate dispenser when draining gasoline from the vapor side of the VST hose.**
5. The fueling point shall be removed from service when VST system pressure drops exceeding the following conditions as determined by Methodology 1 of TP-201.4:  
  
5.00 inches WC at a flow rate of 60 CFH of Nitrogen; and  
8.00 inches WC at a flow rate of 80 CFH of Nitrogen.
6. The fueling point shall be removed from service when the dispensing rate is greater than ten (10) gallons per minute (gpm) or less than five (5) gpm as determined by the applicable provisions of section 6 or 7 of Exhibit 5 or by direct observation for 30 seconds minimum at the maximum hand held position.
7. The fueling point shall be removed from service when any hose has a visible opening as determined by direct observation.
8. The fueling point shall be removed from service when the insertion interlock mechanism allows dispensing when the bellow is uncompressed as determined by direct observation or GDF-09 (see Vapor Recovery Defects List).
9. The fueling point shall be removed from service when the nozzle automatic liquid shut-off mechanisms malfunction in any manner as determined by EPO No. 26-F (See Vapor Recovery Defects List) or direct observation.
10. The fueling point shall be removed from service when any nozzle has a defective vapor valve as determined by Exhibit 10 or when the vapor valve has a leak rate that exceeds

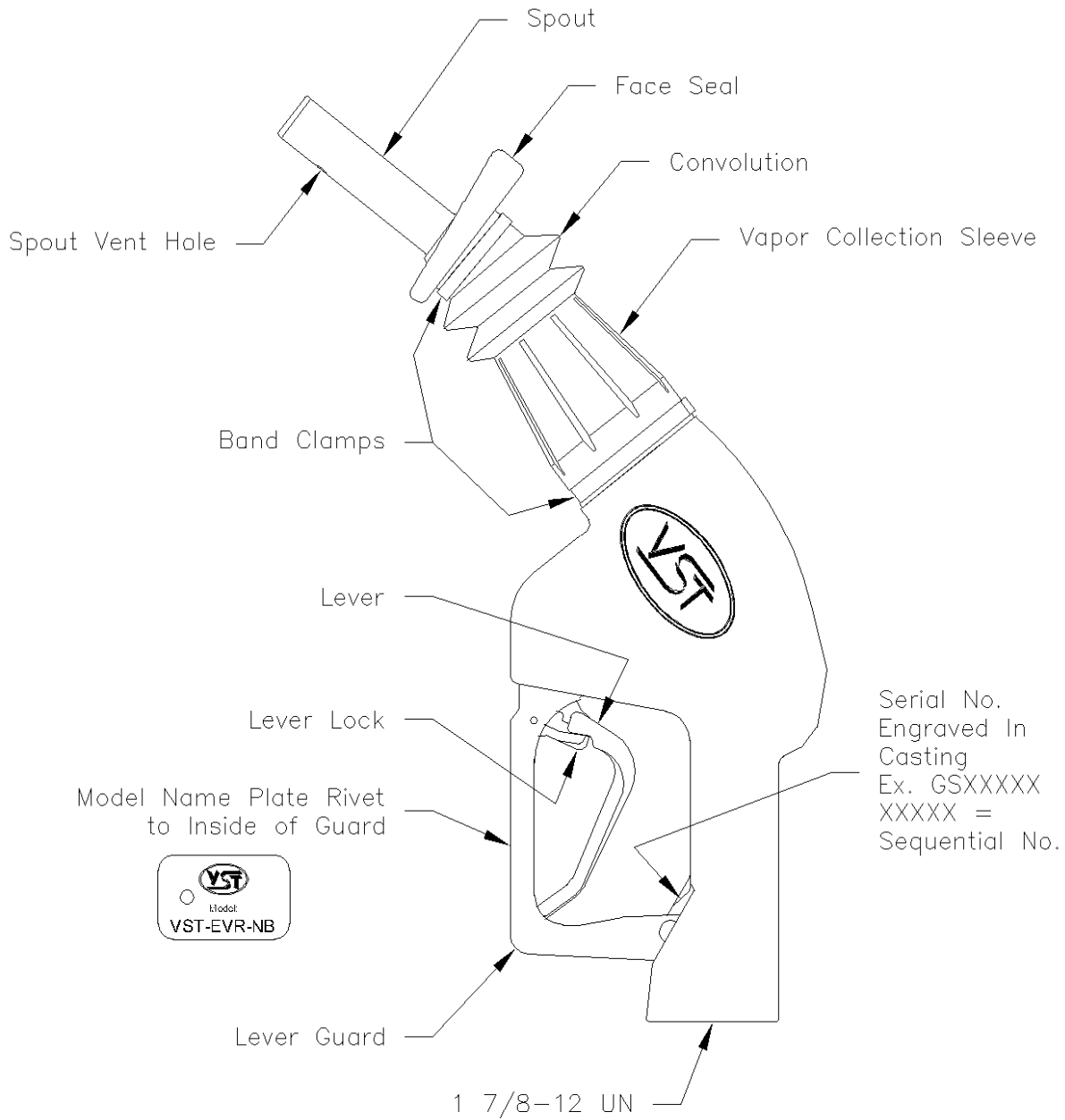
0.07 cubic feet per minute at a pressure of two (2) inches WC as determined by TP-201.2B.

11. The fueling point or system shall be removed from service when any component required by this Executive Order is absent, installed improperly or disconnected as determined by direct observation.

System with VST ECS Processor

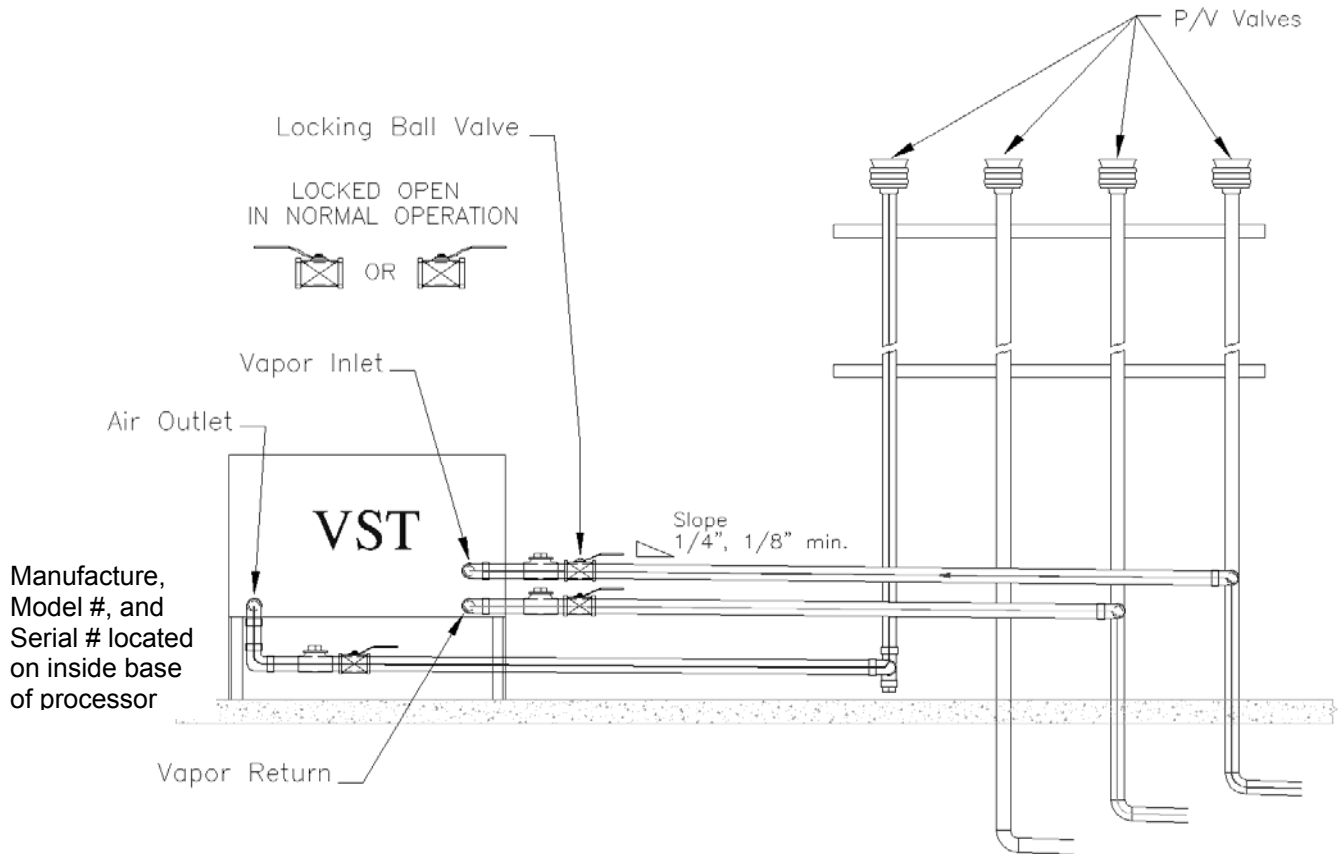
12. The system shall be removed from service when the three ball valves on the VST ECS processor are not locked in the proper operating configuration (Figure 2B-2) as determined by direct observation.
13. The system shall be removed from service when the ECS membrane processor is not on or in the automatic vapor processor mode as determined by the Diagnostic section of the Pressure Measurement Control (Section 16) of IOM.
14. The system shall be removed from service when the VST ECS Processor alarms for emission factor are activated for two consecutive 24 hour periods as determined by direct observation.
15. The system shall be removed from service if the processor fails to activate when the UST pressure is less than or equal to 0.4 inches WC ( $\leq 0.4$  inches WC) as determined by Exhibit 9.
16. The system shall be removed from service when the hydrocarbon concentration of the VST ECS Processor exceeds twelve percent (12%) as found in the Vapor Processor Status Report.

**Figure 2B-1**  
**Model VST-EVR- NB Nozzle**



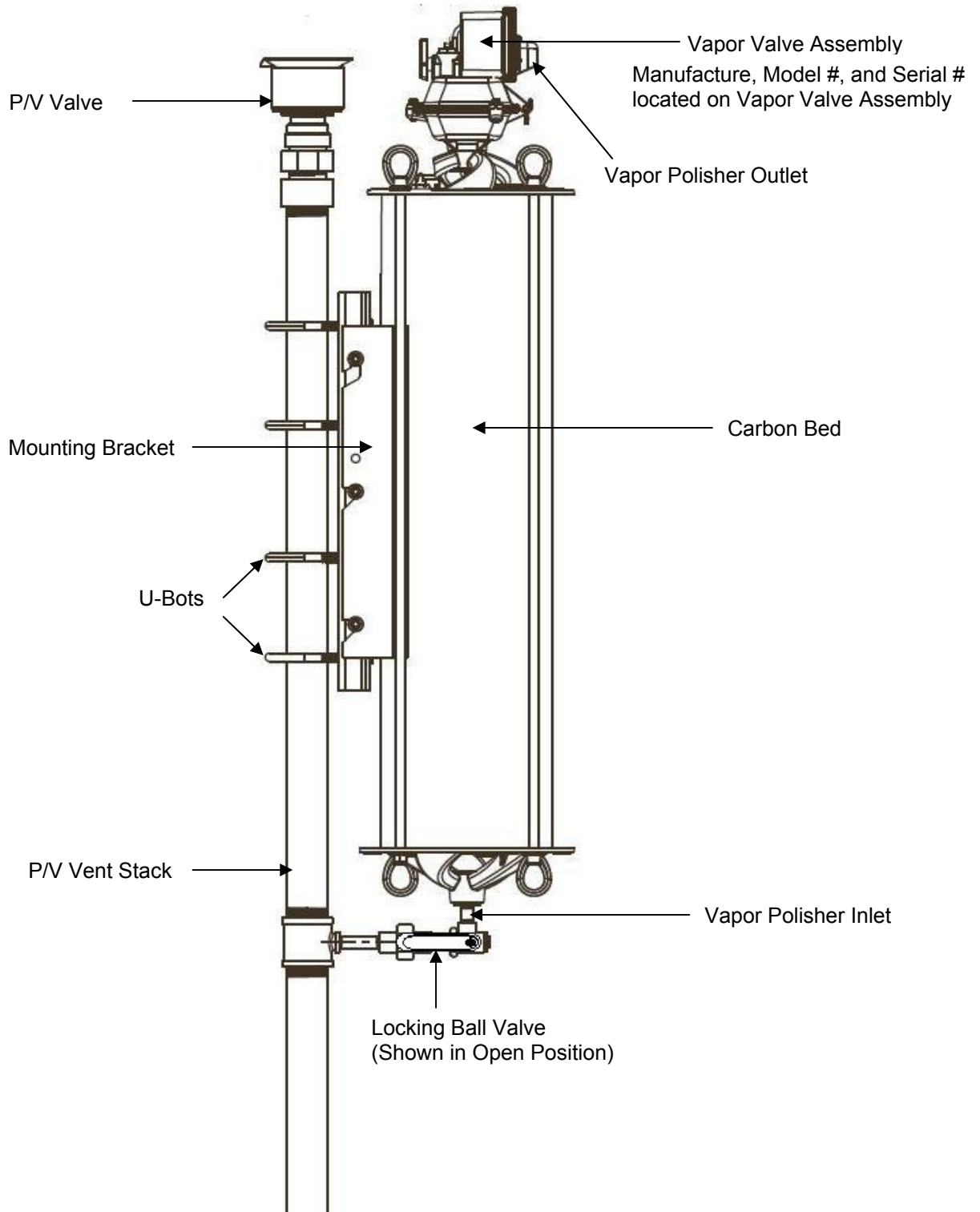


**Figure 2B-2**  
**Typical VST-ECS-CS3 Membrane Processor**



CAUTION: THE HANDLES ON THE LOCKING BALL VALVES MUST NOT BE REMOVED.

Figure 2B-3  
Typical Veeder-Root Vapor Polisher



**Figure 2B-4**  
**Example of a GDF Maintenance Record and Alarm History Record**

Date of Maintenance/ Test/Inspection/Failure/ alarm history (including date and time of maintenance call)	Repair Date To Correct Test Failure	Maintenance/Test/Inspection Performed and Outcome/Action Taken in Response to Alarm	Affiliation	Name and Technician ID Number of Individual Conducting Maintenance or Test	Telephone Number